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**UV and simulated solar photodegradation of 17 $\alpha$ -ethynylestradiol in secondary-treated wastewater by hydrogen peroxide or iron addition**

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1 **Abstract**

2 The extensive use of estrogens and their release, through various pathways, into the  
3 environment, constitutes an emerging environmental problem that poses serious threats onto  
4 public health. In this work the efficiency of UVC/H<sub>2</sub>O<sub>2</sub> and solar/Fe<sup>2+</sup> treatment to degrade  
5 17 $\alpha$ -ethynylestradiol (EE2) in environmentally relevant concentrations of 100  $\mu$ g/L in  
6 secondary-treated wastewater matrices was investigated. Also, photolytic treatment was  
7 performed under different irradiation sources, namely UVC, UVA and simulated solar light.  
8 The effect of H<sub>2</sub>O<sub>2</sub> (0 – 20 mg/L) and Fe<sup>2+</sup> (0 – 15 mg/L) concentration was investigated and,  
9 at optimal operating parameters, EE2 removal was 100% after 15 min of UVC/H<sub>2</sub>O<sub>2</sub>  
10 treatment, while EE2 removal reached 86% after 60 min of solar/Fe<sup>2+</sup> treatment. In addition,  
11 the effect of water matrix and pH was studied. Total organic carbon (TOC) and yeast  
12 estrogen screening (YES) measurements showed the formation of stable intermediate  
13 products during EE2 treatment and an attempt to elucidate the reaction pathways and  
14 mechanisms through the identification of transformation products (TPs) by means of UPLC–  
15 MS/MS was made. Several TPs, including quinone methide and 1,2-quinone derivatives,  
16 were identified and competing pathways were suggested, in which hydroxylation, alkylation,  
17 dealkylation, demethylation and dehydroxylation, amongst others were described as major  
18 transformation mechanisms.

19

20 **Keywords:** wastewater; UVC; solar; estrogen; transformation products; pathways

21

## 1 **1. Introduction**

2 Endocrine disrupting compounds (EDCs) is an emerging environmental issue that poses  
3 serious threats to human beings. EDCs have the ability to interact with the endocrine system  
4 of organisms and either mimic or inhibit the action of animal endogenous hormones, thus  
5 leading to a variety of developmental and reproductive disorders, as well as feminizing  
6 effects [1]. Estrogens include natural, synthetic, and phyto-estrogens and are well-known  
7 EDCs. Of them, synthetic estrogens, such as  $17\alpha$ -ethynylestradiol (EE2), which is the basic  
8 component of the contraceptive pill, are generally more stable than natural estrogens in  
9 aqueous environment and have greater estrogenic potency (approx. 11–27 times) than the  
10 natural estrone (E1) and estradiol (E2) [2]. Recent in vivo studies showed that EE2 even in  
11 the order of  $\mu\text{g/L}$  was able to affect continuously exposed rats, by decreasing their  
12 bodyweight, accelerating vaginal opening, and altering estrous cycles in young animals [3].  
13 Also, chronic exposure to environmentally relevant concentrations of EE2 could cause liver  
14 and gill lesions in zebrafish [4], depress gonadal growth in males mummichogs [5], and could  
15 affect the pituitary transcriptome in female salmon in previtellogenic stages of ovarian  
16 growth, altering the expression of hundreds of genes involved [6].

17 EE2 can enter into aqueous environments (i.e. surface and ground water bodies) through  
18 several pathways, such as wastewater treatment plants (WWTPs), septic systems, and after  
19 use in agriculture [7]. Besides, EE2 is resistant to biological oxidation and escapes intact  
20 from conventional WWTPs, thus accumulating in the environment [8]. Several studies have  
21 reported the occurrence of EE2 in WWTP effluents worldwide (in the range of  $\text{ng/L}$ ), while  
22 even more studies have detected EE2 at surface and drinking water raising serious concerns  
23 for public health [7, 8]. All these findings indicate that current treatment processes at  
24 WWTPs are inadequate to completely remove EE2. Hence, additional or alternative  
25 processes should be applied to support existing WWTP and increase their efficiency.

26 Due to the effectiveness of UV light for disinfecting drinking water, many water treatment  
27 plants are installing UV based systems. Such UV systems may also be effective for treatment  
28 of chemical contaminants, although their ability to destruct them completely is still under  
29 investigation. Nasuhoglu et al. [9] reported that EE2 can be degraded by about 90% and 50%  
30 in pure water and in industrial wastewater matrices, respectively, after 30 min of UVC  
31 treatment. Other studies also showed that UVC has the potential to effectively destruct EE2  
32 in the order of  $\text{mg/L}$  by UVC [10-12], UVC/ $\text{TiO}_2$  [11], UVC/ $\text{H}_2\text{O}_2$  [12, 13] or UV/ $\text{Fe}^{3+}$  [10]  
33 systems. However, more work has to be done to further optimize UV process and assess its  
34 efficiency to treat environmentally relevant EE2 concentrations in real wastewater matrices.

1 Another effective, low-cost and robust alternative that can be used as an additional or as a  
2 tertiary treatment in existing WWTPs, is the use of solar-driven photocatalytic processes.  
3 These seem to be the most suitable treatment technology for using natural sunlight; an  
4 abundant and free source of energy [14]. The role of iron in environmental chemistry was  
5 first reported in the 1990s and since then, several studies on the photo-assisted  $\text{Fe}^{2+}$ , mainly  
6 in the form of the Fenton reagent (i.e.  $\text{Fe}^{2+}/\text{H}_2\text{O}_2$ ), for water treatment applications were  
7 published [14]. Iron can play a dominant catalytic role in organics degradation under natural  
8 environmental conditions. Also, iron is an abundant and non-toxic element and it can be  
9 found at concentrations between 0.5 and 50 mg/L in natural fresh waters, while it does not  
10 present a hazard to human health at levels up to 2 mg/L in drinking water [15]. The  
11 decomposition of EE2 by photo-Fenton process under simulated solar irradiation has been  
12 studied by Frontistis et al. [15] who found that solar photo-Fenton (5 mg/L  $\text{Fe}^{2+}$ /8.6 mg/L  
13  $\text{H}_2\text{O}_2$ ) treatment could completely remove 70  $\mu\text{g/L}$  EE2 from wastewater matrix after only 6  
14 min of treatment. Moreover, estrogens degradation by UV/ $\text{Fe}^{3+}$  [10] treatment system was  
15 studied and showed that the addition of iron can significantly enhance photolytic processes.  
16 The aim of this work is to investigate the degradation of EE2 by UVC and solar irradiation.  
17 Environmentally relevant EE2 concentrations at the  $\mu\text{g/L}$  level are used, while emphasis is  
18 given on EE2 degradation in secondary-treated WWTP effluents. Additional materials, such  
19 as  $\text{H}_2\text{O}_2$  and  $\text{Fe}^{2+}$  to support the photolytic process are used and operating parameters,  
20 including pH, EE2 initial concentration, concentration of peroxide or iron, water matrix and  
21 treatment time are investigated. In addition, transformation products are identified and  
22 potential EE2 degradation pathways are proposed. It should be noted that up to now, a limited  
23 number of studies exist with regard to the transformation products of EE2 [16-20] and that  
24 the photocatalytic degradation of EE2 proves to be a quite complex process due to the stable  
25 structure of the molecule even against such powerful oxidation processes.

26

## 27 **2. Materials and Methods**

28 For this work,  $17\alpha$ -ethynylestradiol (EE2) (>98%, Fluka),  $\text{H}_2\text{O}_2$  (35% w/w, Merck) and  
29 humic acid (Sigma-Aldrich, CAS number: 57-63-6) were purchased and used as received.  
30 EE2 (chemical formula:  $\text{C}_{20}\text{H}_{24}\text{O}_2$ ) is a white to creamy white, odourless crystalline powder  
31 with a molecular mass of 296.40 g/mol and its chemical structure is shown in Figure 1. Its  
32 solubility in water is  $9.20 \pm 0.09 \text{ mg}\cdot\text{L}^{-1}$  at  $25.0 \pm 0.5 \text{ }^\circ\text{C}$  [21] and its octanol-water  
33 partitioning coefficient ( $K_{ow}$ ) is 3.67 [22]. To add, EE2 in distilled water has a maximum  
34 absorbance in UV-Vis electromagnetic spectrum at 221 nm [16].

1  $\text{Fe}^{2+}$  is added in the aqueous solutions in the form of  $\text{FeSO}_4 \cdot 7\text{H}_2\text{O}$  ( $\geq 99\%$ , Sigma-Aldrich).  
2 The wastewater (WW) matrix is collected from the outlet of the secondary treatment of the  
3 municipal WWTP of Chania, Greece. The effluent's TOC content is 7.8 mg/L, its inherent  
4 pH is about 8 and its conductivity is 820  $\mu\text{S}/\text{cm}$ . Ultrapure water (UPW) at pH = 6.1 is taken  
5 from a water purification system (EASYpureRF – Barnstead/Thermolyne, USA).  
6 Commercially available bottled water is used as the drinking water matrix for this study.

7  
8 Figure 1

9  
10 In each photocatalytic run, 300 mL of the water matrix spiked with the appropriate amount of  
11 EE2 and other chemical substances if required, are fed in the photochemical reactor.  
12 Magnetic stirring is always provided and temperature is kept constant at  $25 \pm 2^\circ\text{C}$ , while the  
13 reactor is open to the atmosphere. In those cases when hydrogen peroxide was used, residual  
14  $\text{H}_2\text{O}_2$  was scavenged, in withdrawn samples, adding the appropriate amount of  $\text{Na}_2\text{SO}_3$   
15 ( $\geq 98\%$ , Sigma-Aldrich).

16 UVA and UVC experiments are conducted in an immersion well, batch type, laboratory scale  
17 photoreactor, purchased from Ace Glass (Vineland, NJ, USA) which is described in detail  
18 elsewhere [23]. UVA irradiation is provided by a 9 W lamp (Radium Ralutec, 9W/78, 350–  
19 400 nm). UVC irradiation is provided by an 11 W low pressure mercury lamp (Phillips, TUV  
20 PL-S). The photon fluxes of the UV lamps are determined actinometrically using the  
21 potassium ferrioxalate method and they are estimated at  $4.69 \times 10^{-6}$  einstein/s and  $7.15 \times 10^{-6}$   
22 einstein/s for the UVA and UVC lamp, respectively. Simulated solar irradiation is emitted by  
23 a Newport 96000-150 Watt solar simulator system. Light source is placed on top of a double-  
24 walled cylindrical pyrex cell containing the aqueous reactant mixture. The photon flux of the  
25 solar lamp was measured using 2-nitrobenzaldehyde (purchased from Sigma–Aldrich) as the  
26 chemical actinometer [24] and it was found to be  $17.4 \times 10^{-8}$  einstein/s.

27 Changes in EE2 concentration are followed by an HPLC (Alliance 2690, Waters) system  
28 where separation is achieved on a Luna C-18(2) column (5  $\mu\text{m}$ , 250 mm  $\times$  4.6 mm) and a  
29 security guard column (4 mm  $\times$  3 mm), both purchased from Phenomenex. Detection is  
30 achieved through a fluorescence detector (Waters 474) and method details are described in  
31 detail elsewhere [15]. Analyses of transformation products (TPs) of EE2 photodegradation  
32 were performed by ultra performance liquid chromatography coupled with tandem mass  
33 spectrometry on an ACQUITY TQD UPLC-MS/MS system (Waters) by a method described  
34 in detail elsewhere [16]. Sample extraction was performed by solid phase extraction (SPE)

1 using cartridges built of hydrophilic and a lipophilic monomer (Oasis-HLB; 50 mg/3mL), and  
2 purchased from Waters (Milford, MA, USA). The sample (10 mL) is filtered through a  
3 syringe-filter (22  $\mu$ m pores) prior to the SPE. TOC is measured on a Shimadzu 5050A TOC  
4 analyzer. EE2 absorbance spectrum is measured on a Shimadzu UV-Vis 1240  
5 spectrophotometer. Residual H<sub>2</sub>O<sub>2</sub> concentration was monitored using Merck peroxide test  
6 strips in the range 0–25 mg/L. Finally, the *in vitro* yeast estrogen screen (YES) bioassay was  
7 employed to assess estrogenic activity of the effluent before, and after treatment [15].

8

### 9 **3. Results and Discussion**

#### 10 **3.1. Irradiation source**

11 The effect of the type of the irradiation is investigated using three different illumination  
12 systems, namely UVC, UVA and simulated solar irradiation. The results in Figure 2 show  
13 that the extent of the EE2 degradation follows the order of UVC > UVA > solar. Specifically,  
14 EE2 removal is 47%, 17% and 2% under UVC, UVA and solar irradiation, respectively after  
15 60 min. In general, photolysis can occur by two ways; (i) directly through light absorption by  
16 the organic molecules, and (ii) indirectly when photosensitizers, such as TOC, absorb the  
17 light and generate reactive oxidant species (ROS) that promote molecule degradation [25]. In  
18 this work, the higher EE2 removal percentage under UVC irradiation can be explained both  
19 by its direct and indirect photolytic degradation. Firstly, the emission spectra of the lamps and  
20 the absorbance spectrum of EE2 should be taken into consideration. Measurements (data not  
21 shown) of the UV-Vis spectrum of EE2 show that it absorbs in the 200-300 nm range, with  
22 two significant absorption peaks at 230 nm and 280 nm. The UVC lamp emits at 254 nm, the  
23 UVA lamp emits in the 350 – 400 nm range (max. emission at 365 nm), and the solar  
24 irradiation consists of only about 5% of UVA (i.e. 300 – 500 nm) radiation, while the rest  
25 95% illuminates in the Vis-IR electromagnetic spectrum. Therefore, only the UVC lamp  
26 emits in the absorbance spectrum of EE2, thus initiating its direct photolysis. Besides,  
27 indirect photolysis also takes place since all experiments, shown in Figure 2, are carried out  
28 in WW matrix with a TOC content of 7.8 mg/L. TOC can absorb UV irradiation and form  
29 ROS, thus enhancing EE2 degradation.

30 Moreover, the high performance of the UVC system can be also attributed to the higher  
31 photon flux that finally reaches the reactant solution. As the photon flux in the solution  
32 increases, the amount of photo-generated ROS in the effluent will be increased as well. In  
33 this work, the measured photon fluxes (shown in brackets) of the lamps follow the order of  
34 UVC ( $7.15 \times 10^{-6}$  einstein/s) > UVA ( $4.69 \times 10^{-6}$  einstein/s) > solar ( $17.4 \times 10^{-8}$  einstein/s),

1 indicating the key role of photons' amount in the photolytic process. It should be noted that  
2 the geometrical characteristics of the photo-reactors can significantly affect the process  
3 efficiency. This is evident in this work, where fully immersed designs (i.e. UVC and UVA  
4 systems) allow optimal photon flux diffusion into the solution, while when the lamp is placed  
5 on top of the liquid, such as in the case of solar irradiation, the amount of photon flux in the  
6 solution is less than for the other illumination systems.  
7 Further experiments are focused on the use of both UVC, which is already a widely applied  
8 disinfection technique in WWTPs, and on solar irradiation, a free and renewable source of  
9 energy, to explore the possibility of establishing a more sustainable and advanced treatment  
10 process in existing WWTPs.

11  
12 Figure 2  
13

### 14 **3.2. UVC/H<sub>2</sub>O<sub>2</sub> treatment**

15 To enhance the EE2 degradation extent under UVC irradiation, the addition of 1 – 20 mg/L  
16 H<sub>2</sub>O<sub>2</sub> in WW is investigated and the results are shown in Figure 3. As can be seen, EE2 is  
17 completely and rapidly destructed after only 15 min of treatment, in the presence of 10 mg/L  
18 H<sub>2</sub>O<sub>2</sub>. Also, it is observed that the presence of hydrogen peroxide up to 10 mg/L could  
19 significantly enhance the degradation of EE2, while further increase of its concentration to 20  
20 mg/L does not significantly affect process efficiency. Similar findings have been reported by  
21 other studies [15, 26, 27], yet the investigation of hydrogen peroxide addition in  
22 environmentally relevant EE2 matrices, under UVC irradiation, had been a missing element  
23 in literature. In general, hydrogen peroxide is expected to promote UVC photolysis as it  
24 absorbs in the range of 200 – 290 nm and yields hydroxyl radicals which could then enhance  
25 EE2 indirect photolytic degradation [23, 26]. On the other hand, hydrogen peroxide can also  
26 react with hydroxyl radicals, thus scavenging the photo-generated ROS in the effluent that  
27 would otherwise be available for EE2 destruction. This phenomenon is likely to occur to an  
28 appreciable extent at increased H<sub>2</sub>O<sub>2</sub> loadings and can explain the almost stable EE2 removal  
29 observed at 20 mg/L H<sub>2</sub>O<sub>2</sub> concentration. It should be noted that a significant amount of H<sub>2</sub>O<sub>2</sub>  
30 was consumed during the process since its residual concentration was 2 and 5 mg/L after the  
31 end of treatment, when the initial H<sub>2</sub>O<sub>2</sub> loading was 10 mg/L and 20 mg/L, respectively.  
32 Therefore, all subsequent experiments under UVC irradiation were performed in the presence  
33 of 10 mg/L H<sub>2</sub>O<sub>2</sub>.



Figure 3

To get a better understanding of the EE2 degradation during UVC/H<sub>2</sub>O<sub>2</sub> treatment, the effect of initial EE2 concentration (50 – 200 µg/L) on the process efficiency is investigated. Concentration – time profiles are followed (data not shown) and it is observed that the reaction followed a pseudo-first-order rate expression. Specifically, after only 10 min of UVC/H<sub>2</sub>O<sub>2</sub> treatment at 10 mg/L H<sub>2</sub>O<sub>2</sub>, EE2 removal is 100%, 92% and 82% when initial EE2 concentration is 50 µg/L, 100 µg/L and 200 µg/L, respectively. Besides, the respective apparent k values are 0.293 min<sup>-1</sup> (r<sup>2</sup>=0.995), 0.247 min<sup>-1</sup> (r<sup>2</sup>=0.98) and 0.179 min<sup>-1</sup> (r<sup>2</sup>=0.983).

### 3.3. Solar/Fe<sup>2+</sup> treatment

Solar irradiation is currently promoted for water treatment since it is a cheap and renewable source of energy and it has been used both for bacteria inactivation [28] and water decontamination [29]. Yet, and as shown in Figure 2, solar irradiation alone cannot compete, in terms of its effectiveness, with other photolytic processes. In addition, ferrous ion in acidic aqueous solutions can be photolyzed under appropriate irradiation to produce hydroxyl radicals and other strong non-selective oxidants [10]. These radicals may react with EE2, thus enhancing its degradation as well as oxidizing the natural organic matter (NOM) present in WW matrices. To investigate this, experiments are carried out under solar irradiation while adding up to 15 mg/L Fe<sup>2+</sup> in WW at pH=3, in order to avoid iron precipitation [10]. The results are shown in Figure 4. It is observed that the addition of iron can significantly promote the 60-min photodegradation of EE2 at 26%, 36%, 46% and 86%, in the presence of 1 mg/L, 2.5 mg/L, 5 mg/L and 15 mg/L Fe<sup>2+</sup>. Therefore, solar/Fe<sup>2+</sup> photocatalytic oxidation might be an attractive method to increase the effectiveness of the solar photolytic process. In addition, a final experiment was carried out in the presence of 5 mg/L Fe<sup>2+</sup> and 10 mg/L H<sub>2</sub>O<sub>2</sub> to assess the efficacy of the solar photo-Fenton process to remove 100 µg/L EE2 from treated WW. It is observed that after only 15-30 min of treatment, EE2 is completely degraded, while in the absence of H<sub>2</sub>O<sub>2</sub> the respective EE2 removal is only 35%. As expected, solar photo-Fenton can rapidly destruct EE2, yet for large-scale applications photo-Fenton might be non-sustainable since it requires the addition of two chemical reagents to support the process.

Figure 4

1

2 Furthermore, a series of experiments at different EE2 concentrations are performed under  
3 solar irradiation and in the presence of 5 mg/L Fe<sup>2+</sup> (data not shown). Conversion decreases  
4 with increasing EE2 concentration, i.e. the 60-min value was 53%, 46% and 38% at 50 µg/L,  
5 100 µg/L and 200 µg/L EE2 concentration, respectively.

6

### 7 **3.4. Effect of the water matrix**

8 The use of ultrapure water solutions to simulate natural aqueous matrices is often a limitation  
9 of most laboratory studies. This is because natural waters contain dissolved and suspended  
10 substances, coming from animal and plant materials break down and usually referred to as  
11 NOM. The presence of NOM and of other inorganic substances can affect estrogens' photo-  
12 degradation either positively or, most commonly, negatively [24, 25, 30]. Therefore, in this  
13 work the effect of water matrix onto 100 µg/L EE2 degradation is investigated both for  
14 solar/Fe<sup>2+</sup> and UVC/H<sub>2</sub>O<sub>2</sub> treatments (Figure 5). Experiments are performed in several water  
15 matrices, such as ultrapure water (UPW), secondary-treated wastewater (WW), 10 mg/L  
16 humic acid (HA) solution (HA is one of the main NOM components) and a 50:50 mixture of  
17 WW:UPW. Firstly, it should be reported that EE2 photolytic degradation, under either solar  
18 (without iron) and UVC (without peroxide) irradiation, is almost negligible, at approximately  
19 5-14% (data not shown) for all the experimental conditions (i.e. 15 min under UVC or 60 min  
20 under solar irradiation) described in Figure 5. Moreover, it was observed that TOC removal  
21 of WW, in the presence of EE2 which barely contributes to total TOC, was always below  
22 10% (data not shown) for both UVC/H<sub>2</sub>O<sub>2</sub> and solar/Fe<sup>2+</sup> treatment (i.e. for the experimental  
23 conditions shown in Figures 3 and 4). The almost negligible TOC removal shows the highly  
24 recalcitrant nature of the real WW matrix.

25

26

Figure 5

27

28 As can be seen in Figure 5a, water matrix affects the process efficiency at least at the initial  
29 stages of oxidation. More specifically, EE2 removal is lower in WW and in HA than in UPW  
30 matrix. Interestingly in all cases EE2 is completely removed after 15 min of UVC/H<sub>2</sub>O<sub>2</sub>  
31 treatment showing the capacity of this process to destruct recalcitrant micro-contaminants,  
32 such as EE2, in WWTP effluents. Figure 5b shows that EE2 removal is decreased in complex

1 water matrices as this is 78%, 70%, 59%, and 46% in UPW, drinking, HA, and WW matrix,  
2 respectively, after 60 min of solar/Fe<sup>2+</sup> treatment. Similar results were found during the  
3 heterogeneous photocatalytic degradation of EDCs [16, 24, 31]. This is due to the fact that  
4 the non-selective photo-generated ROS are competitively consumed by the NOM present in  
5 treated WW, which contains 7.8 mg/L of TOC. Since NOM is known to be refractory to  
6 biological or chemical oxidation and constitutes most of the matrix's total organic content,  
7 non-selective oxidizing agents will partly be wasted attacking this fraction [31], thus reducing  
8 the degradation rate of the target compound. Also, hydroxyl radicals may be scavenged by  
9 bicarbonates and chlorides present in WW or HA to form other ROS, whose oxidation  
10 potential is lower than that of the hydroxyl radicals [32].

11

12

### 13 **3.5. Effect of pH**

14 The effect of pH on the process efficiency is studied and a series of experiments are carried  
15 out at pH values of 3, 5 and 8 to destruct 100 µg/L EE2 in treated WW. The results are shown  
16 in Figure 6. It is observed (Figure 6a) that increased pH values can increase the degradation  
17 efficiency of the UVC/H<sub>2</sub>O<sub>2</sub> treatment achieving 92%, 82% and 67% EE2 removal after 10  
18 min at pH values of 8 (i.e. effluents' ambient pH), 5 and 3, respectively. These results are  
19 consistent with those obtained in other studies [33], where a pH increase from 5 to 8 led to a  
20 substantial increase of EE2 photolytic removal, indicating that changes in pH may affect the  
21 formation rate of reactive oxygen species. Undeniably, the higher EE2 removal at pH 8,  
22 which is the ambient pH of natural water bodies, is an additional benefit to the utilization of  
23 UVC/H<sub>2</sub>O<sub>2</sub> treatment for EE2 removal in WW matrix. On the other hand, solar/Fe<sup>2+</sup> process  
24 efficiency is enhanced at low pH values (Figure 6b), i.e. EE2 degradation is 17%, 32% and  
25 46% at pH values equal to 8, 5 and 3, respectively. These findings are consistent with other  
26 studies [10] and this is due to the fact that iron precipitates at pH>4, and therefore less  
27 amount of soluble iron is available to produce hydroxyl radicals for EE2 oxidation. Also,  
28 bicarbonates, well known radical scavengers, at pH 3 may be transformed into gaseous phase  
29 as CO<sub>2</sub>, which is eventually emitted to atmosphere, thus allowing more radicals to oxidize the  
30 target compounds.

31

Figure 6

32

### 1 **3.6. Mineralization and estrogenicity removal**

2 For the various experiments performed in this work, changes in TOC were monitored  
3 alongside EE2 conversion. For the UVC/H<sub>2</sub>O<sub>2</sub> system, TOC reduction never exceeded 11%,  
4 and this is even lower (6%) for the solar/Fe<sup>2+</sup> system. These results clearly show that  
5 although EE2 is degraded, other very recalcitrant intermediate organic products are generated  
6 either from EE2 cleavage or from DOC degradation. Not only this, but measurements of the  
7 effluent's estrogenic activity showed that although complete estrogen degradation is achieved  
8 after 15 min of UVC/H<sub>2</sub>O<sub>2</sub> treatment (Figure 3), this is accompanied by a partial estrogenicity  
9 removal of just 35%. These results show that the photolytic transformation of EE2, as well as  
10 that of the wastewater organic matter, can generate certain stable by-products that are  
11 estrogenically potent and responsible for most of the remaining estrogenicity. Similar  
12 discrepancies between estrogen and estrogenicity removal during treatment by photo-Fenton  
13 oxidation or heterogeneous photocatalysis have been recently reported [15, 33].

14

### 15 **3.7. Formation of TPs and proposed transformation pathways of EE2**

#### 16 3.7.1. Solar/Fe<sup>2+</sup> process

17 Figure 7a illustrates the postulated chemical structures and the exact mass values of the  
18 detected ions for the degradation products identified, during the EE2 solar/Fe<sup>2+</sup> degradation  
19 process. Overall, the screening of the treated samples allowed to tentatively identify the  
20 formation of fourteen TPs (TP1-TP14), with their peaks being greater than 15% of the  
21 highest peak intensity. Even though transformation mechanisms similar to those suggested by  
22 other studies, are proposed herein, some transformation products have not been previously  
23 reported, indicating that a plethora of TPs may occur depending on the experimental and  
24 analytical set up. The structure of most TPs of EE2 shows preservation of the core structure  
25 of the estrogens which can potentially explain the remaining estrogenicity after treatment or  
26 at least part of it. TP1 with m/z 301 (RI 30-70%) is possibly formed from the addition of four  
27 hydrogen atoms to EE2. TP2 (181 m/z, RI 20-80%) and TP3 (149 m/z, RI 15-55%) are  
28 formed from the cleavage of C-C bond from the main structure of EE2, in accordance to the  
29 transformation pathway of EE2. Therefore, the elucidation of these possible structures of TPs  
30 could also result in the removal of few carbon atoms from the hydrocarbon side chains. The  
31 formation of TP2 and TP3 indicates the cleavage of the C11-C12 and C9-C10 bond of EE2 as  
32 a preferential route, which was originated from a series of C-C cleavage products such as the  
33 formation of 2,4a,9,10-tetrahydrophenanthrene and 5,6,7,8-tetrahydro-2-naphthol (THN),  
34 respectively. More specifically, TP2 and TP3 can be formed by the combination of the

1 dehydroxylation, demethylation at the position C12 and finally abstraction of alkyl group,  
2 cyclopentane and octahydro-1H-indene, respectively. The THN molecule was previously  
3 used as a model for steroid hormone photodegradation studies [17, 34]. TP3 can be formed  
4 through two reaction routes of EE2→TP3 and EE2→TP2→TP3. TP3 can be directly formed  
5 from EE2 but can be also generated through two reactions, hydroxylation and abstraction of  
6 cyclohexa-1,4-diene of the TP2. For this reason, TP2 can be regarded as the promoter for the  
7 formation of TP3 (m/z 149). In this study, TP6, TP11 and TP12 are some of the major  
8 transformation products formed after the treatment, which may be attributed to the  
9 hydroxylation of EE2. Several isobaric compounds (polyhydroxylated compounds),  
10 corresponding to positional isomers, may be formed. However, differentiation of positional  
11 isomers was not always feasible based solely on the UPLC-MS/MS data. More specifically,  
12 the degradation of EE2 could lead to the formation of di-hydroxylated photoproducts (2-HO-  
13 EE2), TP6 (m/z 403), TP11 (m/z 329) and TP12 (m/z 305). As previously observed by  
14 Frontistis et al. [33] during the TiO<sub>2</sub> photocatalytic degradation of EE2 one of the major TPs  
15 was TP11 with 329 m/z (RI 15-60%), which may be generated after di-hydroxylation of the  
16 aromatic ring, whose further loss the ethynyl moiety would yield TP12 (m/z 305, RI 40-  
17 80%). The formation of dihydroxy photoproducts, 2-HO-EE2, possibly comes from the attack  
18 of hydroxyl radicals on the aromatic rings [16, 17, 33] [18]. Nevertheless, it is worth  
19 mentioning that TP11 and TP12 are the most frequently identified oxidation TPs of E2 and  
20 EE2 using various advanced oxidation processes [16, 33, 35]. In contrast, the analogous  
21 photoproduct with 329 m/z which may be formed with direct attack of OOH radicals and the  
22 photoproduct with 327 m/z which can be formed with abstraction of two hydrogen atoms  
23 were not observed, as previously reported [16, 19, 20]. TP6 can be formed through the  
24 reaction route of EE2→TP5→TP6. The elucidation route of TP6 can be attributed to the di-  
25 hydroxylation, abstraction methyl group at C-11 of the structure and finally further addition  
26 of hydrogen atoms at ethynyl group of the TP5.

27 Dealkylation is one of the major photooxidation mechanisms that it is observed in the present  
28 study. In contrast with Mazellier et al. [17], TP13 (m/z 273, RI 30-100%) may be formed  
29 with abstraction of alkyl group at position C17, whose further reduction would yield TP14  
30 (m/z 271, RI 40-80%).

31 Alkylation of the aliphatic ring of EE2 also occurs resulting in the formation of five major  
32 analogues of EE2, TP5 (m/z 351, RI 15-50%), TP7 (m/z 449, RI 25-45%), TP8 (m/z 337, RI  
33 15-60%), TP9 (m/z 493, RI 20-55%) and TP10 (B) (377 m/z, RI=15-50%). The formation of  
34 these photoproducts may be attributed to the alkylation on the one of the aliphatic ring at C-7

1 and C-8 positions and elimination of the hydrogen atoms, while TP7 can be generated by the  
2 combination of demethylation at the position C12, and finally alkylation at position C-7 and  
3 C-8 through TP6. Finally, another analogue, TP4 ( $m/z$  227, RI=25-55%) contains multiple  
4 structural changes consistent with the ethynyl moiety liberation at the position C-17 of the  
5 structure together with demethylation and dehydroxylation processes.

6

7

Figure 7

### 8 3.7.2. UVC/H<sub>2</sub>O<sub>2</sub> process

9 Figure 7b presents the eleven TPs (TP1\*-TP11\*) identified and the proposed reaction  
10 pathway of EE2 degradation during the UVC photolytic treatment. Six of the eleven proposed  
11 TPs (TP2\*, TP5\*-TP8\*, TP10\*) are the same with those observed during the solar/Fe<sup>2+</sup>  
12 treatment.

13 Several TPs (TP1\*(A)-(B), TP7\* and TP9\*) are formed through the hydroxylation step.  
14 TP1(A)\* ( $m/z$  331), TP1\*(B) ( $m/z$  331), TP7\*( $m/z$  403) and TP9\* ( $m/z$  314) are the major  
15 transformation products formed during this mechanism. Subsequent hydroxyl radical addition  
16 could lead to the formation of mono- (TP1(B)\*,  $m/z$  331 and TP9\*,  $m/z$  314) and  
17 bihydroxylated (TP1\*(A),  $m/z$  331 and TP7\*,  $m/z$  403) products. As seen in Figure 7b,  
18 several isobaric compounds corresponding to positional isomers are detected. However,  
19 differentiation of positional isomers is not feasible based solely on the UPLC-MS/MS data.  
20 More specifically, TP1(A)\* ( $m/z$  331; RI 30-100%) can be formed through the loss of two  
21 hydrogen atoms and subsequent addition of two hydroxyl radicals onto the saturated ring  
22 linked to the aromatic one in the structure of EE2. TP1(B)\* can be formed through two  
23 reaction routes of EE2→TP1(B)\* and EE2→TP2\*→TP1(B)\*. TP1(B)\* can be directly  
24 formed by the combination of monohydroxylation onto the saturated ring of the structure and  
25 methylation of EE2. In parallel to hydroxylation, methylation reactions are also demonstrated  
26 by the presence of protonated molecules with addition of hydrogen atoms at ethynyl moiety.  
27 TP1(B)\* can be also generated through one-fold methylation and hydroxylation of the TP2,  
28 which can be regarded as the promoter for the formation of this photoproduct ( $m/z$  331).

29 The formation of TP7\* can occur through monohydroxylation and then by further addition of  
30 a methyl group of TP6\*. The TP9\* ( $m/z$  314; RI 15-55%) can result from the direct attack of  
31 hydroxyl radical at position C-10 of the linked saturated ring on the EE2 structure forming  
32 monohydroxylate-derivative [33]. Chen et al. [36] reported that the frontier electron density  
33 value was higher for the carbon atoms at positions 3 and 10 of the aromatic ring of EE2, with

1 carbon at position 10 having the highest value of electron density of all the atoms in EE2.  
2 This finding is in perfect agreement with the value of the frontier electron density estimated  
3 by Ohko et al. [37], on the structurally similar E2 molecule. These values indicate that the  
4 most probable sites at which an electron would be abstracted by a hole are the carbon atoms  
5 at positions 3 and 10 of the aromatic ring of EE2. Given that there is relatively little steric  
6 hindrance to attack by electrophiles at the aromatic ring of EE2, it can be assumed that C-10  
7 of the structure should be the most favorable site for electrophilic attack [33].  
8 In addition to the assigned product ions, TP2\* at 301 m/z is observed. Frontistis et al. [33]  
9 reported that the identified TP2\* could be possibly generated through the addition of four  
10 hydrogen atoms to EE2.  
11 Subsequently, UVC treatment of EE2 can lead to the formation of two other analogues of  
12 EE2 i.e. TP3\*(A)-(B) with m/z values 251 and TP4\* with m/z values 233. TP3\*(B) (m/z 251;  
13 RI 15-30%) may be formed by cleavage of the aromatic ring of EE2, whose subsequent  
14 decarboxylation following by addition of ethynyl moiety at position C17 gives TP4\*(m/z  
15 233; RI 25-45%) which eventually leads to low molecular weight compounds, corresponding  
16 to aliphatic carboxylic acids and other ring-cleavage compounds. The other analogue,  
17 TP3(A)\* (m/z 251; RI 15-30%), may be formed following two hydroxyl groups liberation,  
18 through C-1 and C-17 and losing methyl moiety from position 12.  
19 UVC photolytic oxidation of EE2 can lead to the formation of four other TPs i.e. TP6\* (m/z  
20 361), TP8\* (m/z 449), TP10\* (m/z 493) and TP11\* (m/z 361). As in the case of the solar/ $F e^{2+}$   
21 process, one of the major mechanisms is the alkylation of the aliphatic ring of EE2. TP6\*(m/z  
22 361, RI 20-40%), TP8\* (m/z 449, RI 15-35%), TP10\* (m/z 493, RI 20-60%) and TP11\* (m/z  
23 361, RI 25-70%) may be formed by alkylation at positions C7 and C8 on the aliphatic ring  
24 next to the saturated ring. TP8\* may be formed through two reaction routes of  
25  $EE2 \rightarrow TP6^* \rightarrow TP8^*$  and  $EE2 \rightarrow TP6^* \rightarrow TP7^* \rightarrow TP8^*$ . Through the second reaction route,  
26 photoproduct with 449 m/z may indicate possible abstraction of two hydroxyl groups,  
27 demethylation and finally addition of octahydro-1H-indene at positions 7 and 8 of TP7\*. The  
28 formation of TP8\* can be also attributed to the one-fold addition of octahydro-1H-indene  
29 group at C7-C8 and subsequent addition of hydrogen atoms at the ethynyl moiety.  
30 Finally, according to the elucidation of EE2 pathway, TP5\* (m/z 227; RI 25-75%) is created  
31 from EE2 after loss of hydroxyl radicals, loss of methyl group at position 12 and loss of the  
32 ethynyl moiety at C-17.

33

#### 1 **4. Conclusions**

2 In this work, the fate of synthetic estrogen hormone EE2 is monitored under UVC irradiation  
3 or simulated solar light in the presence of iron in environmentally relevant matrices. The  
4 selection of these two systems is justified taking into account that (i) several WWTPs  
5 upgrade their disinfection procedures through installing UVC setups, and (ii) natural  
6 attenuation driven by sunlight and iron inherently present in WWTPs (and, indeed, other  
7 water courses) may occur. In a nutshell:

8 1) Although UVC alone can partly remove EE2 at the  $\mu\text{g/L}$  level, the extent of removal is  
9 substantially enhanced with the addition of  $\text{H}_2\text{O}_2$  (which may also serve as disinfectant) at the  
10 low  $\text{mg/L}$  level; since EDCs are, in practice, present at the  $\text{ng/L}$  level, there may be no need  
11 for additional oxidants.

12 2) EE2 is susceptible to degradation by sunlight and iron; the process is sensitive to  
13 parameters such as the concentration of iron and the complexity of the water matrix.

14 3) The estrogenicity associated with the presence of EDCs in complex matrices may not be  
15 completely removed upon the elimination of specific estrogens. This brings forward the need  
16 to monitor the formation of key TPs and evaluate their biological potency. In this work,  
17 UPLC-MS/MS analysis is performed to identify such TPs and propose reaction mechanisms  
18 and pathways.

19

20



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## LIST OF FIGURES

Figure 1. Chemical structure of EE2.

Figure 2. EE2 removal during photolytic treatment for different irradiation systems. Conditions:  $[EE2]_0=100\mu\text{g/L}$ ; wastewater matrix.

Figure 3. UVC treatment of EE2 in the presence of  $\text{H}_2\text{O}_2$  at several concentrations. Conditions:  $[EE2]_0=100\mu\text{g/L}$ ; wastewater matrix.

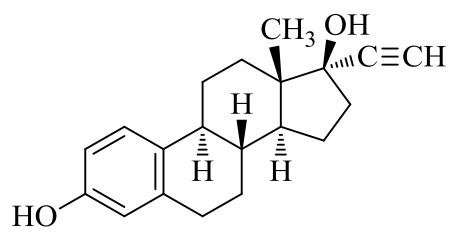
Figure 4. Solar treatment EE2 in the presence of  $\text{Fe}^{2+}$  at several concentrations. Conditions:  $[EE2]_0=100\mu\text{g/L}$ ; wastewater matrix; effluents' pH=3.

Figure 5. Photo-degradation of  $100\mu\text{g/L}$  EE2 in various matrices under (a) UVC/ $\text{H}_2\text{O}_2$  (Conditions:  $10\text{ mg/L H}_2\text{O}_2$ ), and (b) solar/ $\text{Fe}^{2+}$  (Conditions:  $5\text{ mg/L Fe}^{2+}$ ; pH=3) treatment.

Figure 6. Photo-degradation of  $100\mu\text{g/L}$  EE2 at different pH values during (a) UVC/ $\text{H}_2\text{O}_2$  (Conditions:  $10\text{ mg/L H}_2\text{O}_2$ ; WW matrix), and (b) solar/ $\text{Fe}^{2+}$  (Conditions:  $5\text{ mg/L Fe}^{2+}$ ; WW matrix) treatment.

Figure 7. Proposed reaction pathway for the photo-degradation of EE2 in treated secondary WW during (a) solar/ $\text{Fe}^{2+}$  and (b) UVC/ $\text{H}_2\text{O}_2$  treatment.

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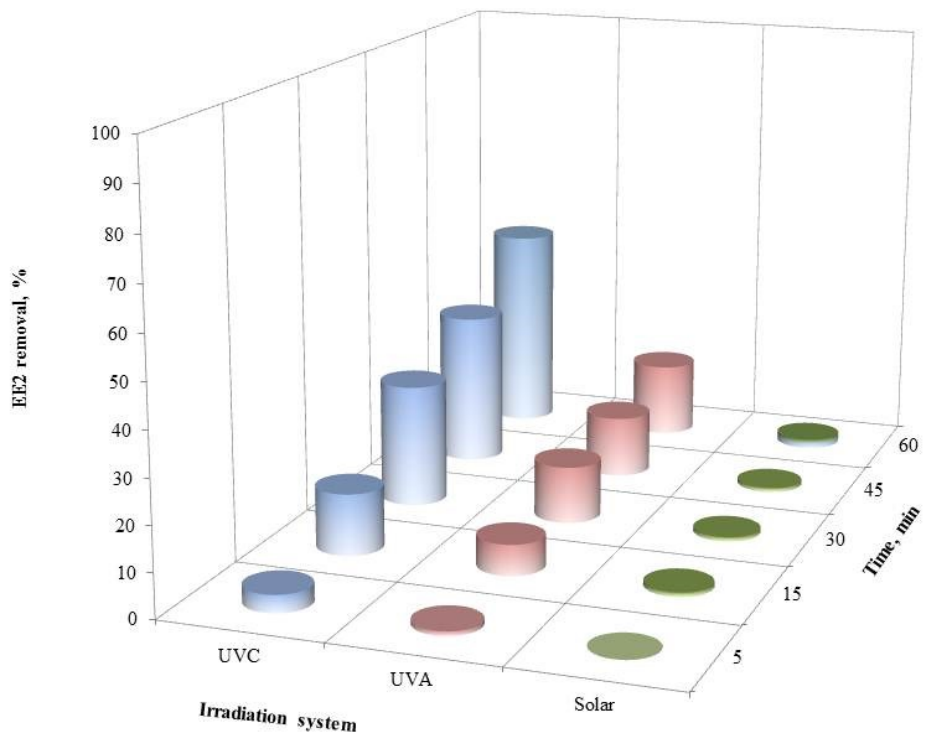


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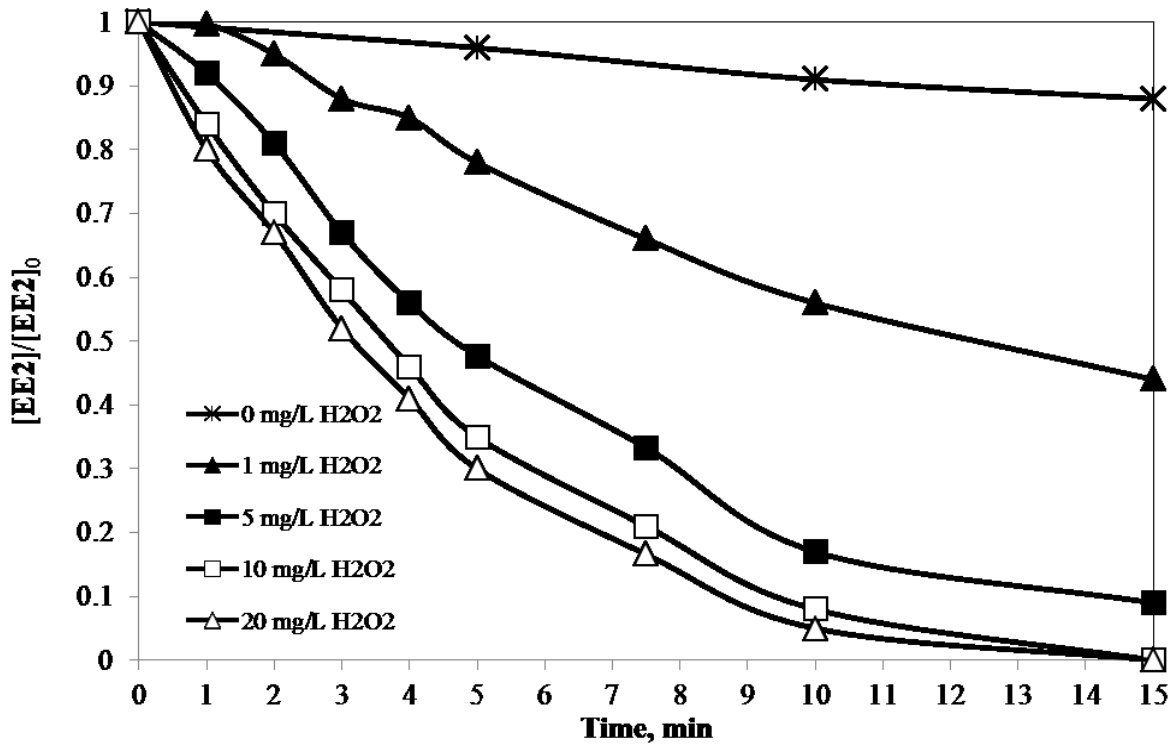
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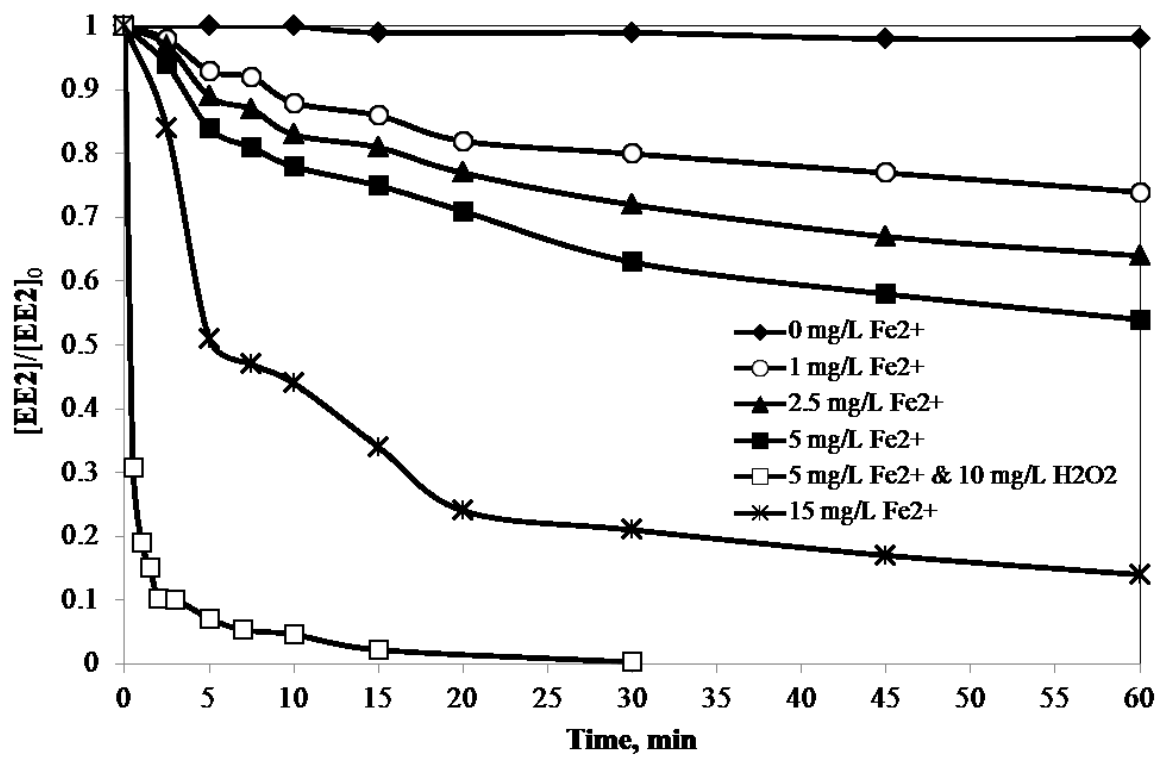
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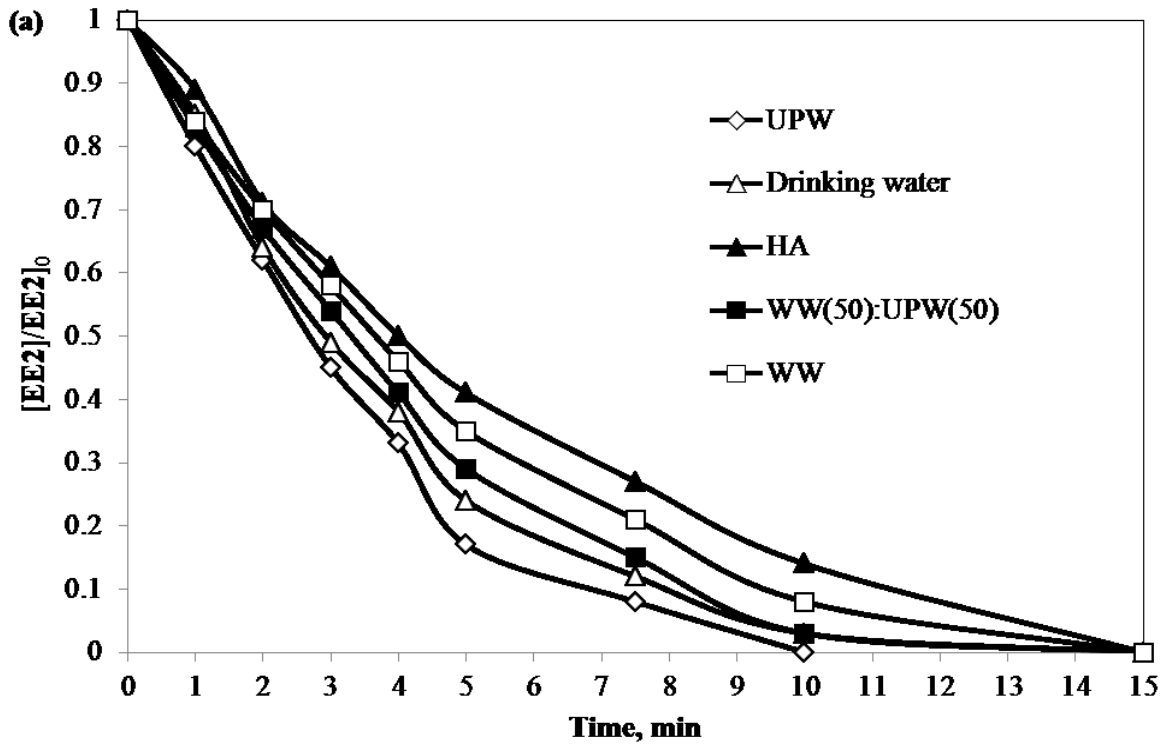


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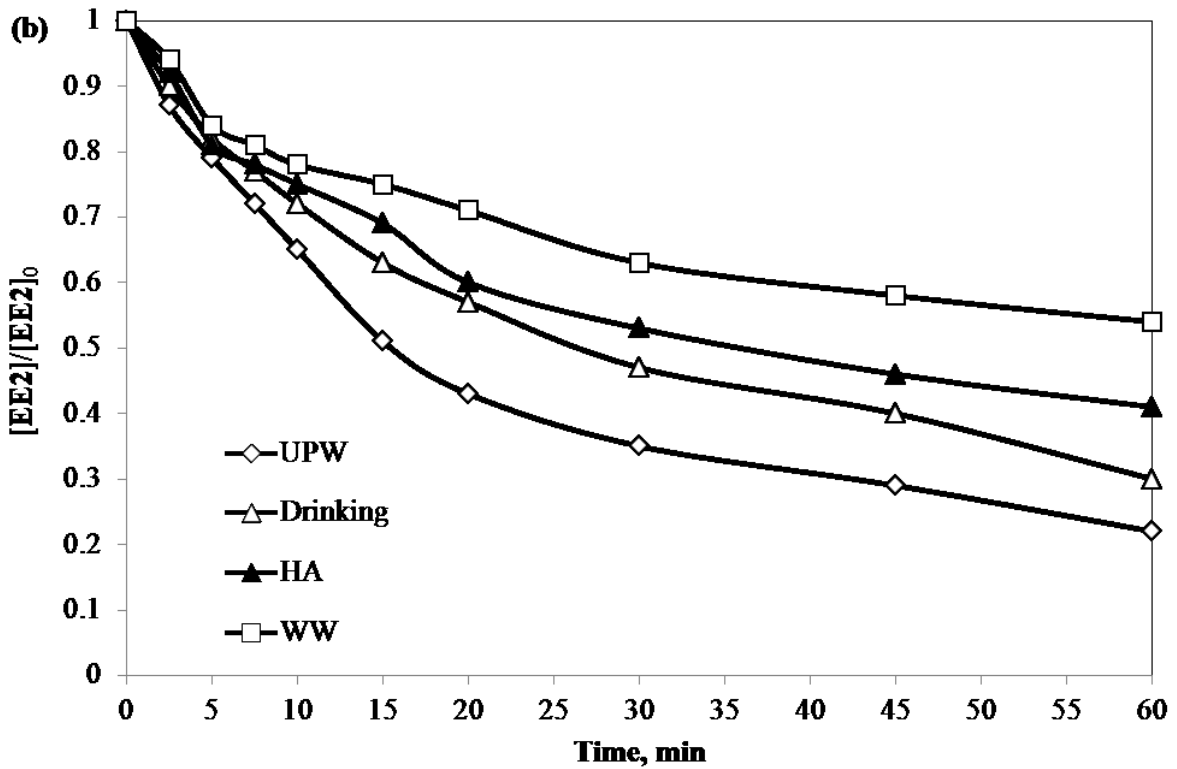
5 Figure 4.



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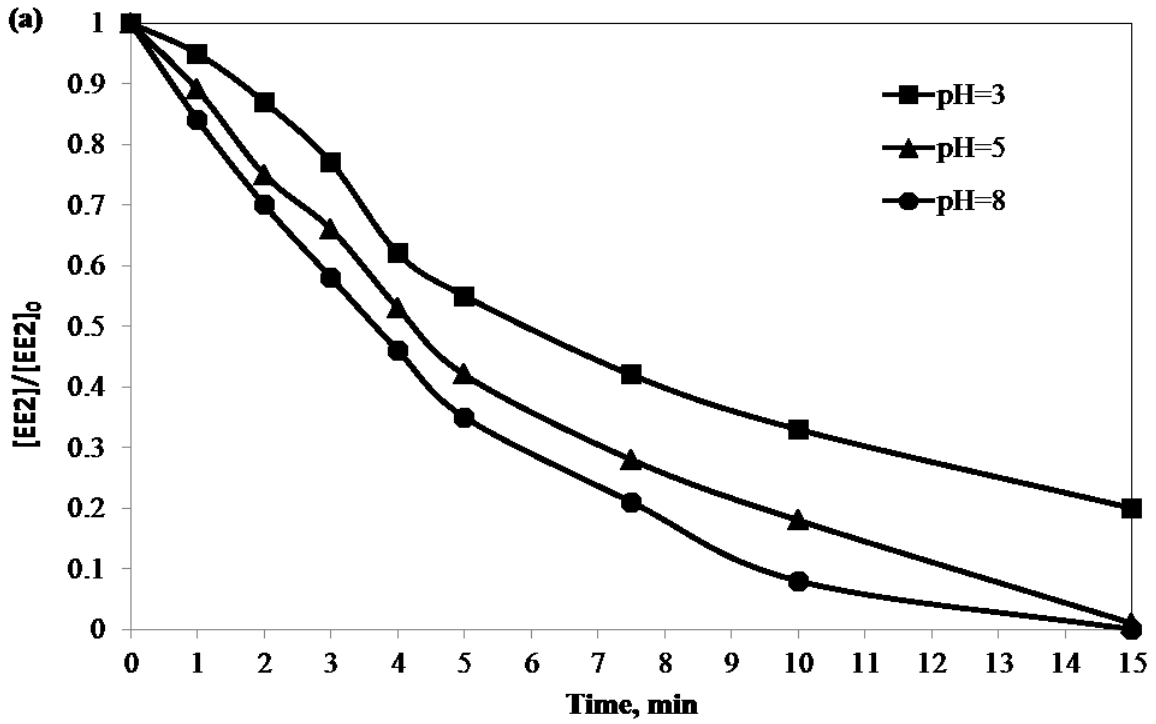
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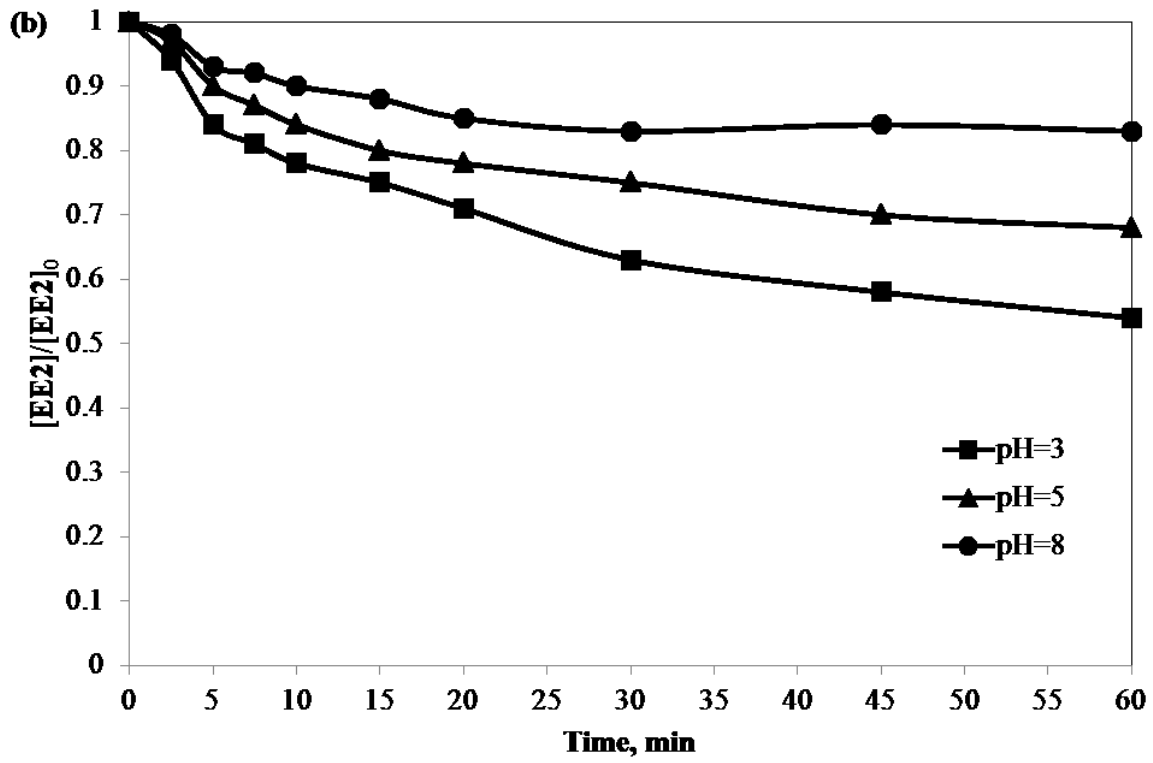
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4 Figure 5.

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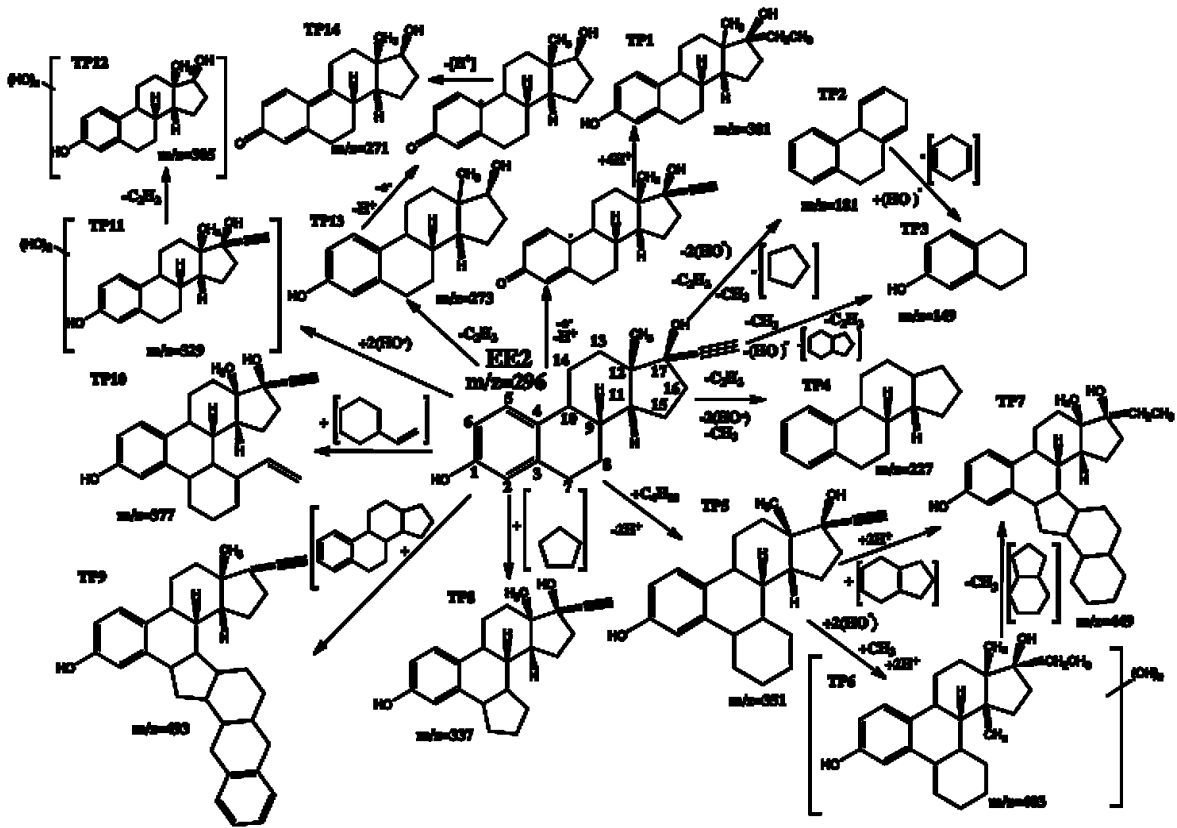
3 Figure 6.

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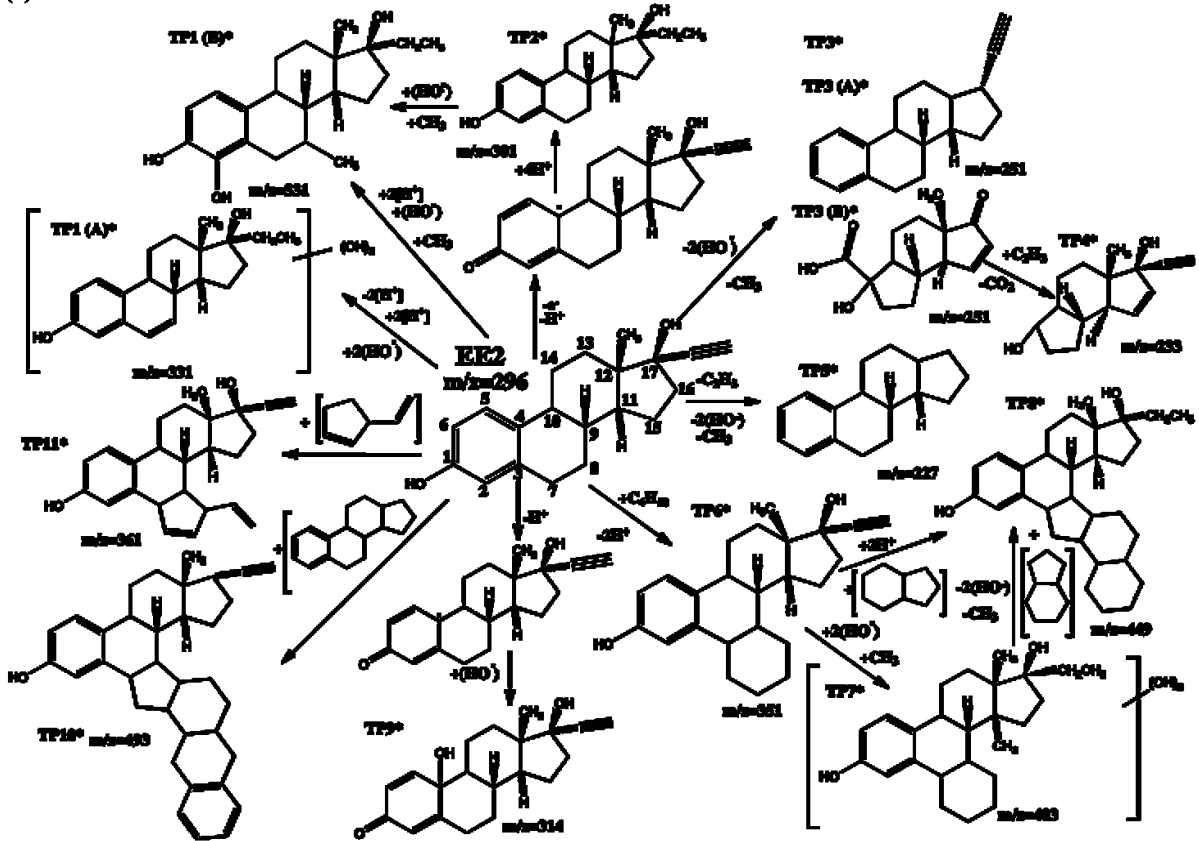
(a)



2

3

(b)



1

2

3 Figure 7.